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Mathematical analysis of high-paraffin oil temperature fields and synthesis of its control system production

Análisis matemático de los campos de alta temperatura de aceite de parafina y síntesis de la producción de su sistema de control

ILYUSHIN, Yury V. 1 & GOLOVINA, Ekaterina I. 2

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ABSTRACT:

Currently, the share of high-paraffin crude oil with high pour points in the balance of hydrocarbon production has significantly increased. In this regard, problems arise in their extraction, preparation, transport and processing, due to a significant increase in viscosity, as well as slump loss at low ambient temperatures. The nature of their course acquires a non-Newtonian character. At the same time, one of the problems that become extremely acute is production and transportation of such hydrocarbon systems. Deep mathematical analysis in this field was made. Keywords: mathematical analysis, temperature field, production, oil.

RESUMEN:

Actualmente, la proporción de petróleo crudo alto en parafina con altos puntos de fluidez en el balance de la producción de hidrocarburos ha aumentado significativamente. A este respecto, surgen problemas en su extracción, preparación, transporte y procesamiento, debido a un aumento significativo en la viscosidad, así como a la pérdida de asentamiento a bajas temperaturas ambientales. La naturaleza de su curso adquiere un carácter no newtoniano. Al mismo tiempo, uno de los problemas que se vuelve extremadamente agudo es la producción y el transporte de tales sistemas de hidrocarburos. Se realizó un profundo análisis matemático en este campo.

Palabras clave: análisis matemático, campo de temperatura, producción, petróleo.

1. Introduction

Hard-to-recover oils are determined by a sufficiently large number of physico-chemical characteristics and one of the factors that classify oils as hard-to-recover among chemical properties is the high paraffin content. It is known that in 2017, 510 million tons of oil was produced in Russia, where more than 75% were oil with high paraffin content. Constant increase in the share of such oils in the total volume of oil produced poses a number of complex technical problems for oil workers [1, mnr.gov.ru].

Paraffin deposit in the bottom-hole formation zone and on the surface of oilfield equipment is one of the serious complications in operation of wells and pipeline transport. Paraffin deposits reduce filtration characteristics of formation, clog pores, reduce the useful section of tubing and, as a

result, significantly complicate production and transportation of oil, increase energy consumption during mechanized production method, and lead to increased deterioration of equipment Ivanova, et al, (2011). Technological processes for extraction, transport and preparation of oil to a large extent depend on the value of viscosities Ivanik, et al, (2018].

Viscosity is the most common characteristic of rheological (flowing) behavior of liquids. For Newtonian objects, it is exhaustive. For non-Newtonian objects, viscosity cannot fully characterize the yield property, but if the substance is processed using "liquid" technological devices and corresponding technology, it can be called "liquideous" and characterize fluidity by a set of effective values Schipachev, et al, (2018].

When transporting oil through a pipeline, a metastable (stable, prone to change) hydrocarbon fluid, prone to release of a solid phase, in the technological range is accompanied by a change in temperature. Transition from a homogeneous fluid to a heterogeneous system means that phase transition has rheological significant consequences and is accompanied by a change in fluidity.

Mechanism of fluidity loss can be different. As a result of «structural solidification», it becomes possible to distinguish various viscosity levels in the object - macroscopic, which determines the flow and mechanical resistance to movement of a large submerged body, and microscopic, which determines, for example, diffusion of low molecular weight components.

Formation of the structure, as a rule, includes several stages. The process begins by interaction of primary particles. Thus, their formation can be considered the first stage. At the second stage, as a result of their interaction, coagulation contacts are formed, and then there is a slow process of their development into phases ones. To date, an opinion has already been formed that dynamics and conditions for appearance of mechanically reversible coagulation contacts determine further evolution of the system. The first stage is weakly manifested in a relatively crude rheological experiment, and the second stage, characterized by non-Newtonian rheological behavior, is highly dependent on hydrodynamic conditions. This leads to the fact that study of thermally induced phase transitions at different strain rates leads to different values of transition temperature.

2. Methodology Existing solution methods

2.1. Existing solution methods

The following methods can be used to combat asphaltene-resin-paraffin deposits (ARPD):

Thermal methods

Technology of using thermophore provides heating the liquid in special heaters - mobile-type boiler plants and supplying it to the well by direct or indirect flushing.

For this purpose, industry produces special units - mobile dewaxing units equipped with boilers liquid heaters up to a temperature of 150 ° C and pumps developing a pressure of up to 16 MPa. The heated agent can circulate in the well for a certain time, providing melt and remove of deposits. The most preferred is backwash, eliminating formation of paraffin plugs, often arising from direct washing.

Electrical dewaxing

One of the methods for dewaxing is the use of devices located in the field of intense paraffin formation. Installation creates a temperature in the range of descent to 100 ° C. Further development of this direction was the descent of heaters inward directly into the paraffin formation intervals, for which a small-sized furnace with a diameter of 29 mm and a power of 9.45 kW was developed.

Heat production due to interaction of chemicals

Creation of a high-temperature thermic field in deposition zone of ARPD is achieved by injection of components interacting with heat generation. At the same time, it is assumed that as a result of exothermic reaction in the cavity, a temperature is created that exceeds the melting temperature of the most refractory components of paraffin deposits. In the capacity of such components, it is proposed to use aqueous solutions of diethylamine and hydrochloric acid. When these components are mixed, an exothermic chemical reaction occurs with the release of a significant amount of heat [Ilyushin, et al, 2017].

Physical methods

Creation of additional crystallization centers. Successful introduction of technologies in recent years used to solve acute problems associated with oil production and based on the use of magnetic effects on field, urgently requires consideration of the mechanism of action of magnetic processing and the effect achieved.

Chemical methods

The process of wax precipitation is a rather complex phenomenon and is characterized by irreversibility of the process. Paraffin crystals that are formed in the oil stream and settle on the walls of the equipment and crystals that occur directly on the surface in contact with oil participate in the formation of deposits. In this regard, the basis of the mechanism for preventing paraffin deposition using protective agent is adsorption processes occurring at the «liquid – solid object» phase boundary.

Mechanical methods and application of facing

The most common method for cleaning lifting pipes from paraffin is mechanical cleaning of pipes with special scrapers, which is performed during operation of wells without stopping it [Martirosyan, 2016]. This method consists of erasure scraps of paraffin deposits from the walls of pipes. Scrapers of various designs are applied. In fountain and compressor wells, downward movement of scrapers is effected by gravity of the scrapers themselves and specially applied loads, and upwards the scrapers are lifted on a steel cable (wire) with a winch. "Flying" scrapers are also used, they are lowered by gravity, and rise without a cable under the influence of energy of an upward flow of a gas-liquid mixture.

2.2. New methodology of solution

To eliminate this problem, small pulse sectional heaters can be installed along the entire plane of producing string and tubing of the transport system. To regulate this system, control device must create effects on the change in temperature field from a given value. Such deviations should be recorded at certain points at a definite time. Then they can be fixed. Thus, it is necessary to calculate the place and time of switching on the heating elements.

The task of stabilizing temperature field is to keep temperature changes T(x, t) within *Tgiv*. This function will be implemented by pulsed heating elements.

This solution is called solution of the heat equation for zero boundary conditions. Consider the control object described by the following mathematical model:

$$T(0,r,t) = T(l,r,t) = 0 ; T(x,R,t) = u(x,t) ; \frac{\partial T(x,0,\tau)}{\partial r} = 0$$
$$\frac{\partial T}{\partial t} = a^2 \left(\frac{\partial^2 T}{\partial x^2} + \frac{1}{r} \frac{\partial T}{\partial r} + \frac{\partial^2 T}{\partial r^2} \right); \ 0 < r < R ; \quad 0 < x < l$$

where T(x,r,t) is the temperature field of control object; a^2 is the specified coefficient of thermal diffusivity of material of control object; R, I are given numbers; u(x,t) - control action, x, r - spatial coordinates of control object; t is time. Output function for this mathematical model will be the function T(x,r,t), where r is a given number from the range (O < r < R). From boundary conditions it is seen that boundaries of the object have zero temperature, input effect is distributed along the boundary of tubing. It is necessary to satisfy condition of temperature field symmetry.

Suppose tubing diameter is negligible. With this assumption, temperature at arbitrary points of an isotropic tubing can be considered the same. We will consider the control object spatially one-dimensional. Then distribution of the temperature field over an isotropic cylinder can be described using the Green's function,

which is infinite Fourier series.
$$T(x, t, \xi, \tau) = \frac{2}{l} \sum_{n=1}^{\infty} \exp\left[-\left(\frac{\pi na}{l}\right)^2 (t-\tau)\right] \sin \frac{\pi n}{l} x \sin \frac{\pi n}{l} \xi$$

where *n* is the number of a member of the Fourier series; *I* – tubing length; *t* – time; *x* is the point (coordinate along the X axis) of location of temperature sensor; ξ is the point (coordinate along the X axis) of heating element location; τ is the moment of switching on the point source, a^2 is the given coefficient of thermal diffusivity of control object material.

Thus, resulting formula allows us to calculate behavior of the temperature field at an arbitrary point of the tubing at an arbitrary point in time. However, to study temperature field over time, it is necessary to obtain the initial heating function.

Since temperature value is the sum of Green's function values at the current time and initial heating condition [Martirosyan, et al, 2016]. Thus, to analyze temperature field, it is necessary to apply a formula that takes into account function of initial condition:

$$T(x_j, t) = \sum_{i=1}^{d} \sum_{n=1}^{k} \frac{2}{l} \exp\left[-\left(\frac{\pi na}{l}\right)^2 t\right] \sin\frac{\pi n}{l} x_j \sin\frac{\pi n}{l} \xi_i + \sum_p \sum_{n=1}^{k} \frac{2}{l} \exp\left[-\left(\frac{\pi na}{l}\right)^2 \left(t - \tau_p\right)\right] \sin\frac{\pi n}{l} x_j \sin\frac{\pi n}{l} \xi_{z(p)}$$

By modeling control system using this function, an observer has ability to monitor the temperature field propagation at any point of one-dimensional control object at any time interval [Martirosyan, 2019]. Thus, resulting formula shows the behavior of temperature field taking into account operating time of the system. This equation is modeled in any programming language and in any software environment.

3. Results

Numerical example

We expand functionality of the proposed methodology for a two-dimensional object, described by the following

mathematical model
$$\frac{\partial T}{\partial t} = a^2 \left(\frac{\partial^2 T}{\partial x^2} + \frac{\partial^2 T}{\partial y^2} + \frac{\partial^2 T}{\partial z^2} \right); 0 < x < l_x$$

$$0 < y < l_y; 0 < z < l_z$$

Boundary and initial conditions of the control object:

$$T(x, y, \tau) = U(x, y, \tau); \quad \frac{\partial T(x, y, 0, \tau)}{\partial r} = 0;$$

$$T(x, 0, \tau) = T(x, l_y, \tau) = T(0, y, \tau) = T(l_x, y, \tau) =; \quad T(x, y, 0) = 0$$

Values of the temperature field, determined using fundamental solution to the problem of heat conduction at zero boundary conditions, that in two-dimensional version will look like:

$$G(x, y, \rho, \mathbf{v}, t) = \frac{4}{l_1 \cdot l_2} \cdot \sum_{k,m=1}^{\infty} \sin\left(\frac{k \cdot \pi \cdot x}{l_1}\right) \cdot \sin\left(\frac{m \cdot \pi \cdot y}{l_2}\right) \cdot \sin\left(\frac{k \cdot \pi \cdot \rho}{l_1}\right) \times \\ \times \sin\left(\frac{m \cdot \pi \cdot \mathbf{v}}{l_2}\right) \cdot \exp\left[-a^2 \pi^2 \cdot t \cdot \left(\frac{k^2}{l_1^2} + \frac{m^2}{l_2^2}\right)\right]$$

In this equation, coordinates of the heating points are x, y, geometric indicators of the control object l_1 , l_2 ; the number of members of the Fourier series k, m; coordinates of the temperature sensor p, v. (Fig. 1)

Figure 1

Next task is to analyze the system when initial time n tends to infinity, t=0, r=0. Influence of the Fourier series will be like this:

$$\exp\left[-a^2\pi^2 \cdot t \cdot \left(\frac{k^2}{l_1^2} + \frac{m^2}{l_2^2}\right)\right] = 1$$

Temperature field results in a spatially distributed control object will look like this:

;

$$T(x, y, \xi) = \frac{4}{l_1 \cdot l_2} \cdot \sum_{k,m=1}^{\infty} \sin\left(\frac{k \cdot \pi}{l_1}\right) x \cdot \sin\left(\frac{k \cdot \pi}{l_1}\right) p \cdot \sin\left(\frac{m \cdot \pi}{l_2}\right) y \cdot \sin\left(\frac{m \cdot \pi}{l_2}\right) v;$$

Impulsive energy source creates a heating pulse at a point $p = v = \frac{1}{4}$, then value of temperature field will have the following form:

$$T(x, y, \xi) = \frac{4}{l_1 \cdot l_2} \cdot \sum_{k,m=1}^{\infty} \sin\left(\frac{k \cdot \pi}{l_1}\right) x \cdot \sin\left(\frac{k \cdot \pi}{4}\right) \cdot \sin\left(\frac{m \cdot \pi}{l_2}\right) y \cdot \sin\left(\frac{m \cdot \pi}{4}\right);$$

For this case, amplitude of Fourier components will be represented like this:
$$A_n = \frac{4}{l_1 \cdot l_2} \left|\sin\frac{\pi p}{4} \cdot \sin\frac{\pi v}{4}\right|.$$

For this case, amplitude of Fourier components will be represented like this:

Only first 5 members are taken. Such conditions can be established: $x = y = \frac{l}{4}$, p = v = 1,2,3,4,5, then:

$$\begin{split} T_1(x,y) &= \frac{4}{l_1 \cdot l_2} \left(\sin \frac{\pi}{4} \sin \frac{\pi}{l_1} x \right) \cdot \left(\sin \frac{\pi}{4} \sin \frac{\pi}{l_2} y \right); \ A_1 = 32 \frac{1}{l^2}; \\ T_2(x,y) &= \frac{4}{l_1 \cdot l_2} \left(\sin \frac{2\pi}{4} \sin \frac{2\pi}{l_1} x \right) \cdot \left(\sin \frac{2\pi}{4} \sin \frac{2\pi}{l_2} y \right); \ A_2 = 64 \frac{1}{l^2}; \\ T_3(x,y) &= \frac{4}{l_1 \cdot l_2} \left(\sin \frac{3\pi}{4} \sin \frac{3\pi}{l_1} x \right) \cdot \left(\sin \frac{3\pi}{4} \sin \frac{3\pi}{l_2} y \right); \ A_3 = 32 \frac{1}{l^2}; \\ T_4(x,y) &= \frac{4}{l_1 \cdot l_2} \left(\sin \frac{4\pi}{4} \sin \frac{4\pi}{l_1} x \right) \cdot \left(\sin \frac{4\pi}{4} \sin \frac{4\pi}{l_2} y \right); \ A_4 = \frac{1}{l^2}; \\ T_5(x,y) &= \frac{4}{l_1 \cdot l_2} \left(\sin \frac{5\pi}{4} \sin \frac{5\pi}{l_1} x \right) \cdot \left(\sin \frac{5\pi}{4} \sin \frac{5\pi}{l_2} y \right); \ A_5 = 32 \frac{1}{l^2}; \end{split}$$

It can be seen from the condition that $G(x, y, \rho, v, t) \ge 0$ for any parameters. Then it is clear that range of positive values of the function in the range of x values will decrease. This narrowing will lead the system to the

region of solutions near point $p = v = \frac{l}{4}$, When $p, v \to \infty$, we get

$$\frac{4}{l_1 \cdot l_2} \cdot \sum_{k,m=1}^{\infty} \sin\left(\frac{k \cdot \pi}{l_1}\right) x \cdot \sin\left(\frac{k \cdot \pi}{l_1}\right) p \cdot \sin\left(\frac{m \cdot \pi}{l_2}\right) y \cdot \sin\left(\frac{m \cdot \pi}{l_2}\right) v$$

generalized function that allows to record a point effect, as well as the spatial density of physical quantities concentrated or applied at one point, i.e.

$$\delta(x-p,y-v) = \frac{4}{l_1 \cdot l_2} \cdot \sum_{k,m=1}^{\infty} \sin\left(\frac{k \cdot \pi}{l_1}\right) x \cdot \sin\left(\frac{k \cdot \pi}{l_1}\right) p \cdot \sin\left(\frac{m \cdot \pi}{l_2}\right) y \cdot \sin\left(\frac{m \cdot \pi}{l_2}\right) v$$

Such a δ^- function represented in the form of Fourier series is considered a generalized function. These functions have a very large application for modeling.

Independent variables are coordinates of the control object

$$\delta(x-p,y-v) = \begin{cases} \infty, & npu \quad y = v \\ 0, & npu \quad y \neq v \\ \infty, & npu \quad x = p \\ 0, & npu \quad x \neq p \end{cases}$$

When considering functions f(x, y), that have extensive distribution $\begin{bmatrix} 0, l_1 \end{bmatrix} \begin{bmatrix} 0, l_2 \end{bmatrix}$, then this equality is unfair:

$$\int_{0}^{l_{1}} \int_{0}^{l_{2}} f(x, y) \delta(x - p, y - v) dx \cdot dy = f(p, v)$$

Pulses limited by flow rate introducing a time δ – function $\delta(t - \tau)$ can be overviewed, function will turn infinity, then

$$\int_{-\infty}^{+\infty} \delta(t-\tau) dt = 1$$

If there is function f(t) , which is defined on the interval $\begin{bmatrix} t_0, t \end{bmatrix}$, then

$$\int_{t_0}^t f(t)\delta(t-\tau)dt = \begin{cases} f(\tau), ecnu & \tau \in [t_0, t]; \\ 0, ecnu & \tau \notin [t_0, t], \end{cases}$$

We get that to describe the function f(x, y, t) and δ -function, presence of three variables is necessary, namely, variable coordinates and time. If application with a relay control principle is applied to a distributed

control object, the output function changes. We apply action at a point P_0 , V_0 at a time, then we get the following function:

$$T(x, y, t) = \int_{0}^{t} \int_{0}^{L_{1}} \int_{0}^{L} G(x, y, t, p, v, \tau) \delta(p - p_{0}) \delta(v - v_{0}) \times \\ \times \delta(\tau - \tau_{0}) dp dv d\tau = G(x, y, t, p_{0}, v, \tau_{0})$$

To make a deeper analysis, we fix the time at a point other than zero. Amplitude of Fourier series components can be analyzed:

$$A_n = \left| \frac{4}{l_1 \cdot l_2} \sin \frac{\pi n}{l_1} p \cdot \sin \frac{\pi n}{l_2} v \cdot \exp \left[-a^2 \pi^2 \cdot t \cdot \left(\frac{k^2}{l_1^2} + \frac{m^2}{l_2^2} \right) \right] \right|_{l_1}$$

When $n \to \infty$, action of each subsequent Fourier series member decreases. This calculation will be based on the given accuracy ε .

if
$$|A_n| \leq \varepsilon$$
, и $\left| \sin \frac{\pi n}{l} \xi(p, v) \right| \leq 1$,

then:

$$\left|\frac{4}{l}\sin\frac{\pi n}{l}\xi(p,\nu)\right| \le \frac{4}{l} \left|\exp\left[-\left(\frac{\pi na}{l}\right)^2 t\right]\right| \le \frac{\varepsilon l}{4},$$
$$\exp\left[\left(\frac{\pi na}{l}\right)^2 t\right] \ge \frac{4}{\varepsilon l} \left(\frac{\pi na}{l}\right)^2 t \ge \ln\frac{4}{\varepsilon l}, n^2 t \ge \left(\frac{l}{\pi a}\right)^2 \ln\frac{4}{\varepsilon l},$$
$$n \ge \frac{L}{\pi a\sqrt{t}} \sqrt{\ln\frac{4}{\varepsilon l}};$$

If accuracy will be calculated, with l = 10, a = 0,01, a = 0,01, $\varepsilon = 0,0001$; then, $n \ge 9.167$ and therefore, if the required accuracy of calculations is provided for system requirements $\varepsilon = 0,0001$, then accuracy of the result will be 91% when calculating nine Fourier series members. It can be noticed that over time, system enters a constant mode of operation and amplitude falls down. After that, Fourier series members will begin to have the least effect. Thus, we calculate the time after which the number of Fourier series members can be reduced.

$$t \ge \left(\frac{l}{\pi na}\right)^2 \ln \frac{4}{\varepsilon l} \cdot t \ge 0.25.$$

The considered model shows temperature field behavior in static regime without taking into account interaction between sources and sensors of the system. We analyze the system in dynamic mode, for this we obtain the control, variable in space, initial heating function. This function will allow to determine temperature field after taking into account effects of all heat sources on the given object; later on, this function will allow to simulate behavior of the temperature field over time. Consider the plane on which n point pulsed sources and *n* sensors are installed and the following boundary conditions are established

The system leaves the state of spacehold under influence of pulsed heating elements with a relay control

principle. All heating elements are switched on simultaneously $\tau_0 = 0$. All of these heating elements will have a temperature effect on all sensors in the system. If we consider the case of influence of all sources on one sensor, then the total action will look like:

$$T(x_{1}, y, t, \tau_{0}) = \sum_{i=1}^{n} \frac{4}{l_{1} \cdot l_{2}} \sum_{k,m=1}^{\infty} \left[-a^{2}\pi^{2} \cdot t \cdot \left(\frac{k^{2}}{l_{1}^{2}} + \frac{m^{2}}{l_{2}^{2}}\right) \right] \cdot \sin\left(\frac{k \cdot \pi \cdot x}{l_{1}}\right) \cdot \sin\left(\frac{m \cdot \pi \cdot y}{l_{2}}\right) \times \\ \times \sin\left(\frac{k \cdot \pi \cdot \rho}{l_{1}}\right) \cdot \sin\left(\frac{m \cdot \pi \cdot v}{l_{2}}\right);$$

Time-varying heating elements create heating pulses to temperature sensors x_1 , x_2 . To analyze annular propagation and inter-pulse interaction, we will calculate behavior of the temperature field near the heating point x(1;1), and coordinates of the temperature sensor p (1; 1). With following input data:

$$l = 10, a = 0.00001, x_1 = \xi_1 = 1, T_{c\dot{a}\ddot{a}} = 0.3, T_{c\dot{a}\ddot{a}} = 0.3, d = 9, \xi_i \in \{1, 2, 3, 4, 5, 6, 7, 8, 9\},$$
$$T(x_1, y_2, t, \tau_0) = \sum_{i=1}^{n} \frac{4}{t_i} \sum_{i=1}^{\infty} \left[-a^2 \pi^2 \cdot t \cdot \left(\frac{k^2}{t_i^2} + \frac{m^2}{t_i^2}\right) \right] \cdot \sin(\frac{k \cdot \pi \cdot x}{t_i}) \cdot \sin\left(\frac{m \cdot \pi \cdot y}{t_i^2}\right) \times \left[-a^2 \pi^2 \cdot t \cdot \left(\frac{k^2}{t_i^2} + \frac{m^2}{t_i^2}\right) \right] \cdot \sin(\frac{k \cdot \pi \cdot x}{t_i^2}) \cdot \sin\left(\frac{m \cdot \pi \cdot y}{t_i^2}\right) \times \left[-a^2 \pi^2 \cdot t \cdot \left(\frac{k^2}{t_i^2} + \frac{m^2}{t_i^2}\right) \right] \cdot \sin(\frac{k \cdot \pi \cdot x}{t_i^2}) \cdot \sin\left(\frac{m \cdot \pi \cdot y}{t_i^2}\right) \times \left[-a^2 \pi^2 \cdot t \cdot \left(\frac{k^2}{t_i^2} + \frac{m^2}{t_i^2}\right) \right] \cdot \sin\left(\frac{k \cdot \pi \cdot x}{t_i^2}\right) \cdot \sin\left(\frac{m \cdot \pi \cdot y}{t_i^2}\right) \times \left[-a^2 \pi^2 \cdot t \cdot \left(\frac{k^2}{t_i^2} + \frac{m^2}{t_i^2}\right) \right] \cdot \left[-a^2 \pi^2 \cdot t \cdot \left(\frac{k^2}{t_i^2} + \frac{m^2}{t_i^2}\right) \right] \cdot \left[-a^2 \pi^2 \cdot t \cdot \left(\frac{k^2}{t_i^2} + \frac{m^2}{t_i^2}\right) \right] \cdot \left[-a^2 \pi^2 \cdot t \cdot \left(\frac{k^2}{t_i^2} + \frac{m^2}{t_i^2}\right) \right] \cdot \left[-a^2 \pi^2 \cdot t \cdot \left(\frac{k^2}{t_i^2} + \frac{m^2}{t_i^2}\right) \right] \cdot \left[-a^2 \pi^2 \cdot t \cdot \left(\frac{k^2}{t_i^2} + \frac{m^2}{t_i^2}\right) \right] \cdot \left[-a^2 \pi^2 \cdot t \cdot \left(\frac{k^2}{t_i^2} + \frac{m^2}{t_i^2}\right) \right] \cdot \left[-a^2 \pi^2 \cdot t \cdot \left(\frac{k^2}{t_i^2} + \frac{m^2}{t_i^2}\right) \right] \cdot \left[-a^2 \pi^2 \cdot t \cdot \left(\frac{k^2}{t_i^2} + \frac{m^2}{t_i^2}\right) \right] \cdot \left[-a^2 \pi^2 \cdot t \cdot \left(\frac{k^2}{t_i^2} + \frac{m^2}{t_i^2}\right) \right] \cdot \left[-a^2 \pi^2 \cdot t \cdot \left(\frac{k^2}{t_i^2} + \frac{m^2}{t_i^2}\right) \right] \cdot \left[-a^2 \pi^2 \cdot t \cdot \left(\frac{k^2}{t_i^2} + \frac{m^2}{t_i^2}\right) \right] \cdot \left[-a^2 \pi^2 \cdot t \cdot \left(\frac{k^2}{t_i^2} + \frac{m^2}{t_i^2}\right) \right] \cdot \left[-a^2 \pi^2 \cdot t \cdot \left(\frac{k^2}{t_i^2} + \frac{m^2}{t_i^2}\right) \right] \cdot \left[-a^2 \pi^2 \cdot t \cdot \left(\frac{k^2}{t_i^2} + \frac{m^2}{t_i^2}\right) \right] \cdot \left[-a^2 \pi^2 \cdot t \cdot \left(\frac{k^2}{t_i^2} + \frac{m^2}{t_i^2}\right) \right] \cdot \left[-a^2 \pi^2 \cdot t \cdot \left(\frac{k^2}{t_i^2} + \frac{m^2}{t_i^2}\right) \right] \cdot \left[-a^2 \pi^2 \cdot t \cdot \left(\frac{k^2}{t_i^2} + \frac{m^2}{t_i^2}\right) \right] \cdot \left[-a^2 \pi^2 \cdot t \cdot \left(\frac{k^2}{t_i^2} + \frac{m^2}{t_i^2}\right) \right] \cdot \left[-a^2 \pi^2 \cdot t \cdot \left(\frac{k^2}{t_i^2} + \frac{m^2}{t_i^2}\right) \right] \cdot \left[-a^2 \pi^2 \cdot t \cdot \left(\frac{k^2}{t_i^2} + \frac{m^2}{t_i^2}\right) \right] \cdot \left[-a^2 \pi^2 \cdot t \cdot \left(\frac{k^2}{t_i^2} + \frac{m^2}{t_i^2}\right) \right] \cdot \left[-a^2 \pi^2 \cdot t \cdot \left(\frac{k^2}{t_i^2} + \frac{m^2}{t_i^2}\right) \right] \cdot \left[-a^2 \pi^2 \cdot t \cdot \left(\frac{k^2}{t_i^2} + \frac{m^2}{t_i^2}\right) \right] \cdot \left[-a^2 \pi^2 \cdot t \cdot \left(\frac{k^2}{t_i^2} + \frac{m^2}{t_i^2}\right) \right] \cdot \left[-a^$$

Then:

$$T(x_1, y_2, t, \tau_0) = \sum_{l=1}^{m} \frac{4}{l_1 \cdot l_2} \sum_{k,m=1}^{n} \left[-a^2 \pi^2 \cdot t \cdot \left[\frac{k}{l_1^2} + \frac{m}{l_2^2} \right] \right] \cdot \sin\left(\frac{k \cdot \pi \cdot x}{l_1}\right) \cdot \sin\left(\frac{m \cdot \pi \cdot y}{l_2}\right)$$

$$\times \sin\left(\frac{k \cdot \pi \cdot \rho}{l_1}\right) \cdot \sin\left(\frac{m \cdot \pi \cdot v}{l_2}\right) = 4,8827000;$$

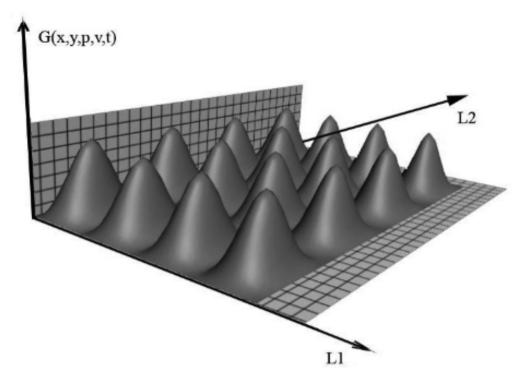
$$T(x_1, y_0, t, \tau_0) = \sum_{i=1}^n \frac{4}{l_1 \cdot l_2} \sum_{k,m=1}^\infty \left[-a^2 \pi^2 \cdot t \cdot \left(\frac{k^2}{l_1^2} + \frac{m^2}{l_2^2} \right) \right] \cdot \sin\left(\frac{k \cdot \pi \cdot x}{l_1}\right) \cdot \sin\left(\frac{m \cdot \pi \cdot y}{l_2}\right) \times \\ \times \sin\left(\frac{m \cdot \pi \cdot v}{l_2}\right) \cdot \sin\left(\frac{k \cdot \pi \cdot \rho}{l_1}\right) = 4,8827316;$$

$$T(x_2, y_1, t, \tau_0) = \sum_{l=1}^n \frac{4}{l_1 \cdot l_2} \sum_{k,m=1}^\infty \left[-a^2 \pi^2 \cdot t \cdot \left(\frac{k^2}{l_1^2} + \frac{m^2}{l_2^2} \right) \right] \cdot \sin\left(\frac{k \cdot \pi \cdot x}{l_1}\right) \cdot \sin\left(\frac{m \cdot \pi \cdot y}{l_2}\right) \times \\ \times \sin\left(\frac{m \cdot \pi \cdot v}{l_2}\right) \cdot \sin\left(\frac{k \cdot \pi \cdot \rho}{l_1}\right) = 4,8827116 ;$$

$$T(x_0, y_1, t, \tau_0) = \sum_{l=1}^n \frac{4}{l_1 \cdot l_2} \sum_{k,m=1}^\infty \left[-a^2 \pi^2 \cdot t \cdot \left(\frac{k^2}{l_1^2} + \frac{m^2}{l_2^2} \right) \right] \cdot \sin\left(\frac{k \cdot \pi \cdot x}{l_1}\right) \cdot \sin\left(\frac{m \cdot \pi \cdot y}{l_2}\right) \times \\ \times \sin\left(\frac{m \cdot \pi \cdot v}{l_2}\right) \cdot \sin\left(\frac{k \cdot \pi \cdot \rho}{l_1}\right) = 4,8827222 ;$$

We display graphically obtained results (Fig. 2), from the graph, total amplitude of the temperature field is visible. However, over time, a temperature drop will occur and it becomes necessary to find a function for dynamically displaying behavior of the temperature field:

Figure 2 The first heating pulse

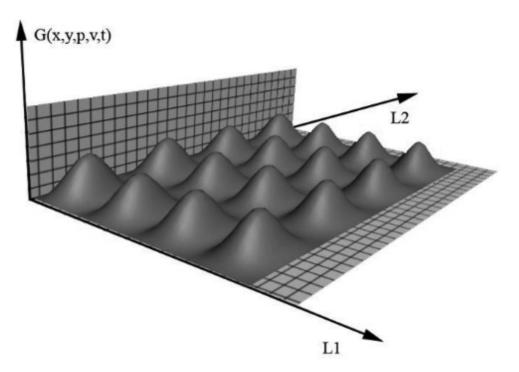


To dynamically display behavior of the thermal field, this function will be used:

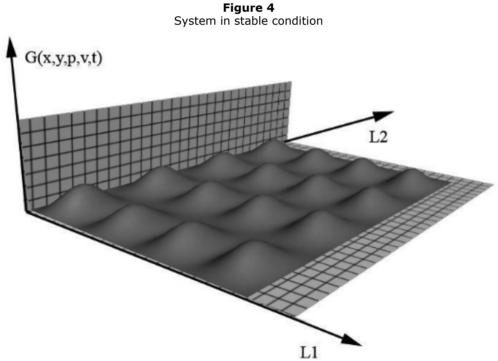
$$\begin{split} T(x_j, y_j, t) &= \sum_{i=1}^d \sum_{k,m=1}^\infty \frac{4}{l_1 \cdot l_2} \exp\left[-a^2 \pi^2 \cdot t \cdot \left(\frac{k^2}{l_1^2} + \frac{m^2}{l_2^2}\right)\right] \cdot \sin\left(\frac{k \cdot \pi \cdot x_j}{l_1}\right) \times \\ &\times \sin\left(\frac{k \cdot \pi \cdot \rho_i}{l_1}\right) \cdot \cdot \sin\left(\frac{m \cdot \pi \cdot y_j}{l_2}\right) \cdot \sin\left(\frac{m \cdot \pi \cdot \nu_i}{l_2}\right) + \sum_p \sum_{k,m=1}^\infty \frac{4}{l_1 \cdot l_2} \times \\ &\times \exp\left[-a^2 \pi^2 \cdot (t - \tau_p) \cdot \left(\frac{k^2}{l_1^2} + \frac{m^2}{l_2^2}\right)\right] \sin\left(\frac{m \cdot \pi \cdot y_j}{l_2}\right) \cdot \sin\left(\frac{k \cdot \pi \cdot x_j}{l_1}\right) \times \\ &\times \sin\left(\frac{k \cdot \pi \cdot \rho_{z(p)}}{l_1}\right) \cdot \sin\left(\frac{m \cdot \pi \cdot \nu_{z(p)}}{l_2}\right); \end{split}$$

Obtained initial condition function is able to determine temperature field behavior over time at any point in the control object. Program code that implements this task had been analyzed before [Kirsanova, Lenkovets, 2016]. Over time, function will take the form:

Figure 3 The system while reaching a stable state



Further system will go to steady state condition. Established temperature regimes will create control actions only at those points of control object Tav = Tgiv, system reaches a stable state. Stable process:



Thus, task of maintaining the temperature field was solved. The state of oil flow and its structure with this method of maintaining heat should be analyzed.

For the object of study, the following characteristics can be taken:

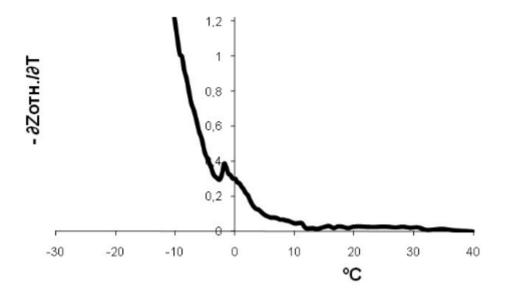
1. Oil from the Sobolinoye field ($\eta = 120 \text{ mPa} \cdot \text{s}, \rho = 0.850 \text{ g}/\text{cm}^3$)

2. Oil of the Archinsky field ($\eta = 125 \text{ MPa} \cdot \text{s}, \rho = 0.860 \text{ g} / \text{cm}^3$).

According to Figure 5, crystallization of paraffin occurs at a temperature of -2 °C.

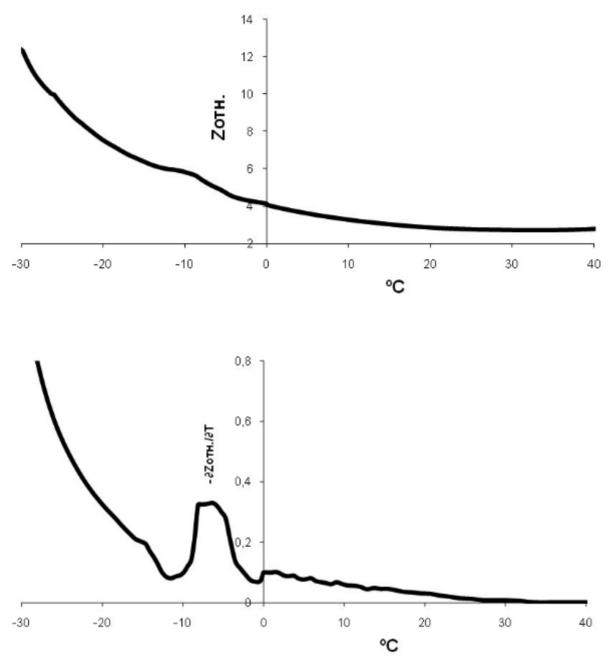
Figure 5

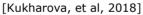
Dependence of mechanical resistance -aZont. / at on temperature of the oil sample of the Sobolinoye field



After adding heating elements, onset of paraffin crystallization is shifted to the low temperature zone by 7 0C, which confirms the effect of heating elements (Fig. 6).

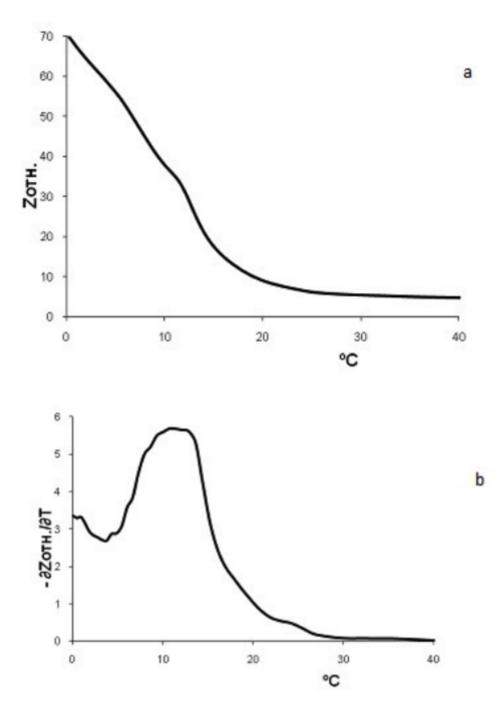
 $\label{eq:Figure 6} \begin{array}{c} \mbox{Figure 6} \\ \mbox{Dependence of mechanical resistance Zrel (a) and ratio -}\partial Zrel / \ensuremath{\partial t} (b) \\ \ensuremath{\text{on temperature of the oil sample of the Sobolinoye field}} \end{array}$





Increase in the content of paraffins in oil disperse systems determines their onset of crystallization in positive temperature ranges. Consider a sample of oil from the Archinsky field with a paraffin content of 6.6%. Figure 7 shows the results of dependence of relative mechanical resistance on temperature.

Figure 7 Dependence of mechanical resistance Zrel. (a) and -∂Zrel. / ∂t (b) on temperature of the oil sample of the Archinsky field [2]



Oil-freezing point occurs at + 10 °C, which creates significant problems when pumping and extracting deposits of this type of oil from the reservoirs.

The onset of paraffin crystallization in oil of the Archinsky field changes insignificantly, 2 0C colder than initial sample. However, in figure 6 b, the second maximum is clearly visible at T=2 0C. This can probably be explained by complex, two-phase crystallization mechanism.

As in the case of Sobolinoye oil deposit, dependencies presented for Archinskaya oil consist of two main linear sections. Moreover, a sharp increase in relative mechanical resistance of oil, which is significantly lower than that of the original sample, is seen.

A sharp increase in Z_{rel} of initial sample begins at T = 19 - 20 °C. After introduction of additives, region of intensive increase in Z_{rel} shifts by 5 - 6 °C and practically repeats the dependence form corresponding to the initial sample (table 1).

Table 1The beginning of oil crystallizationwith addition of dopant

Sample Name	Crystallization temperature,	
	OC	

Sable oil	-2	
With external heating	-10	
Archinskaya oil	10	
With external heating	8	

Source: compiled by Author considering [2, Kukharova, et al, 2018]

Thus, developed methods show the real technical effect of implementation.

4. Conclusions

This paper proposes applied theory and methods for synthesis of distributed, non-linear control objects using example of process of high-paraffin oil extraction. Application of these methods depends not only on time, but also on spatial distribution of the object. In this connection, class of control actions is fundamentally expanding, primarily due to possibility of including in their number four-dimensional guidance described by functions of several variables - time and spatial coordinates.

All advantages of applying the approach make it possible to build control systems in which problems are solved comprehensively taking into account spatiotemporal controls occurring in object under consideration [Samigullin, et al, 2018]. Effectiveness of regulation is provided by dynamic characteristics and response of the system to external disturbances.

The main results of the work are:

• Procedure for stabilizing temperature field based on the Green's function is proposed. This technique consists in reaction of control system to the deviating value of temperature field caused by a pulsed source with a relay control principle. In connection with synthesis of a system with distributed parameters, synthesis of a control system differs from a linear spatial attachment to control object, spatial distribution of input actions and taking into account the spatial interaction of temperature fields [3-20].

• A new procedure for calculating the minimum number of heating elements to stabilize temperature field is proposed. This technique was modeled with a different number of heating elements. It gives the right to argue that proposed methodology solves the problem of temperature stabilization in the oil pipeline and in the screw.

• A software package has been developed; it allows to simulate behavior of a thermal field in an oil pipeline.

The studies presented in this paper are the final stage in development of a temperature field control system for production and transportation of high-paraffin oil.

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1. Associate professor, Department of System Analysis and Control, Saint-Petersburg Mining University, e-mail: Ilyushin_yuv@pers.spmi.ru

2. Associate professor, Department of Economics, Accounting and Finance, Saint-Petersburg Mining University, e-mail: Golovina_EI@pers.spmi.ru

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